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# High-efficiency removal of cationic dye and heavy metal ions from aqueous solution using amino-functionalized graphene oxide, adsorption isotherms, kinetics studies, and mechanism

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Abstract: GO-NH, (amino functionalized graphene oxide) was synthesized by grafting (3-aminopropyl) triethoxysilane onto the surface GO (graphene oxide). The GO-NH, with a higher surface area and many active sites was characterized and its effectiveness in removing Rhod B dye and Ni(II) ions from wastewater by adsorption was observed. The effects of pH, time, and strange ions on the adsorption efficiency were investigated. The equilibrium isotherm data confirmed that it fits the Langmuir and Freundlich isotherm models. GO and GO-NH, exhibited high adsorption capacity (Q<sub>N</sub>); 2500 (mg L<sup>-1</sup>) and 3333 (mg L<sup>-1</sup>) for Rhod B dye, and 312.5 (mg L<sup>-1</sup>), and 714.28 (mg L<sup>-1</sup>) for Ni(II) ions, respectively. The kinetics of adsorption was studied using pseudo-first-order, pseudo-second-order, intraparticle diffusion, and the Boyd model. It was found that the adsorption followed pseudo-second-order and film diffusion model are effective in this adsorption process. Adsorption mechanisms have been attributed to possible electrostatic attractions, hydrogen bonding, and interactions. In summary, the experimental results showed the synthesized GO and GO-NH, would be promising adsorbents to remove aqueous solutions contaminated with Rhod B dye and Ni(II) ions.

Keywords: Adsorption, amino functionalized graphene oxide, grapheneoxide, mechanism, Ni (II) ions, and rhodamine B dye.

# 1. Introduction

Heavy metal ions and organic dyes caused serious concern due to their general coexistence in various industrial wastewater [1]. Rhodamine B (Rhod B) dye and Ni (II) ions in many industries such as rubber, plastics, leather/textile processing plants, industries, electrical contacts, plastic, and battery production are released as waste [2,3]. The presence of these persistent pollutants poses a serious threat to anoxic conditions and human health by affecting the penetration of sunlight, which has a profound effect on photosynthetic activities and aquatic respiration [4]. Adsorption remains the most widely used method to eliminate these emerging threats [5,6]. The use of both raw and fabricated materials as different alternatives in the adsorption process keeps the interest in materials science warm, especially. An ideal adsorbent should have the ability to quickly and efficiently remove toxic pollutants from environments to a safe level [7]. Nanomaterials play an increasingly important role in removing dye and metal ions due to their higher specific surface area and sequestering properties [8,9]. Recently, various nanomaterials are at various stages of research and development, and carbon-based nanomaterials are one of the materials with potential applications in wastewater treatment systems [10].

Graphene and its derivatives have generally been considered highly effective adsorbents due to their ultra-high surface area and numerous surface groups. It is prone to functionalization with different oxygen-containing functional groups such as carboxyl and hydroxyl groups, which can significantly increase its adsorption. The  $\pi$ - $\pi$  stacking and van der wall forces support the adsorption capacity and adsorption capacity of dyes and heavy metals [11,12]. However, there are some disadvantages direct use of GO for wastewater treatment [13]. Both the tendency to aggregate in the layer-by-layer mode due to strong inter-orbital interactions that reduce the adsorption efficiency and the relatively limited number of functional groups are insufficient to remove wastewater pollutants effectively. Also, the oxygen-containing functional groups of GO in coordination with pollutants are not very stable. Recently, to improve the adsorption performance of GO, many researchers have focused on using amino group compounds to functionalize it. Synthesized GO-NH, has more functional groups, surfactant sites, selectivity and separation performance than GO. Thus, aggregation is prevented and the



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selectivity and adsorption capacity of GO against pollutants is increased. [14–17]. In this study, GO-  $NH_2$  was synthesized to remove pollutants from aqueous solutions and studied its effectiveness in adsorption.

This study attempts to investigate the efficacy of GO and GO-NH<sub>2</sub> as an adsorbent for rhodamine B (Rhod B) and Ni(II) ions and their roles in the active site formation in aqueous solution media. Firstly, the synthesized adsorbents were characterized. Then, the optimum conditions were determined to investigate the adsorbent performance in removing rhodamine B (Rhod B) and Ni (II) ions from the aqueous solution and batch adsorption experiments. The equilibrium sorption data were applied to the Langmuir, Freundlich, and Dubinin-Radushkevich isotherm models. Kinetic models were used for evaluating the mechanism and behavior of rhodamine B (Rhod B) dye and Ni(II) ions adsorption onto GO and GO-NH<sub>2</sub>. Desorption results were obtained and a possible adsorption mechanism was evaluated.

# 2. Materials and methods

### 2.1. Synthesis of GO and GO-NH2 adsorbent

Graphene oxide (GO) synthesis: The Hummers Method was used in the synthesis of graphene oxide within the scope of this study (presented in Scheme 1). Five g of graphite, 115 mL of  $H_2SO_4$  (98%), and 2.5 g of NaNO<sub>3</sub> were mixed in an ice bath for 30 min without the temperature exceeding 20 °C. Fifteen g of KMnO<sub>4</sub> was added portion-wise every 30 min to the mixture in the ice bath and stirred for one h. Then it was stirred at 45 °C for 1 h. After this time, 230 mL of distilled water was added and mixed rapidly for another 15 min. After adding 230 mL of water and stirring for 30 min at 45 °C, 600 mL of distilled water and 150 mL of  $H_2O_2$  (9%) were added and mixed for 1 more h, and then washed with HCl (5%) solution prepared with filtered distilled water and dried.

Synthesis of amine functional graphene oxide (GO-NH<sub>2</sub>): One g of graphene oxide was taken into 100 mL of toluene and sonicated in an ultrasonic bath for 30 min. Then, 2.6 mL of 3-aminopropyltriethoxysilane (APTES) was added and stirred for 3 h at room temperature, then refluxed at 100 °C. After cooling to room temperature, the black product was filtered. Then, it was washed with toluene, distilled water and ethyl alcohol and dried under vacuum at 50 °C [18].

### 2.2. Sample characterization

GO examples were analyzed with DR-Uv/Vis (Shimadzu UV-2600 spectrophotometer), XRD (RIGAKU SMARTLABTM X-ray diffractometer) and SEM (scanning electron microscope-TESCAN MAIA3 XMU) and Raman spectra (Renishaw InVia Reflex Raman Microscopy System). Additionally, the FTIR spectra of the GO and GO-NH<sub>2</sub> samples were taken on a Bio-Rad-Win-IR spectrophotometer carrying out KBr discs in between 4000 and 400 cm<sup>-1</sup>.

# 2.3. Preparation of RhB ve Ni (II) ions as adsorbate

In this study, cationic synthetic rhodamine B dye with an acidic alligator (Rhod B) ( $C_{28}H_{31}CIN_2O_3$ ; MA: 479.02 g mol-1; from Merck) is presented in Figure 1 and Ni(NO<sub>3</sub>)<sub>2</sub> 6 H<sub>2</sub>O (MA: 290.79 g mol-1; from Merck) were used. Standard solutions (1000 mg L-1) were prepared to be diluted at different concentrations.



Scheme 1. Synthesis protocol of GO and GO-NH<sub>2</sub>.



Figure 1. Structure and absorbance plots for Rhod B.

#### 2.4. Adsorption experiments

Experiments were performed at 298 K using the standard batch adsorption procedure. The absorbance value of the remaining Rhod B dye solution was determined with a UV-vis spectrometer (Model Hitachi-2800), and the concentration of Ni(II) ions was determined using an AAS (atomic absorption spectroscopy) (Thermo Scientific ICE-3000). The calibration curve and absorbance of the dye concentration were determined to evaluate the amount of dye present in the adsorption samples. The absorbance of the Rhod B dye solution was measured on a Shimadzu UV-1800 spectrophotometer at a wavelength of 554 nm. The removal percentage (% R) was calculated using Equation (1) to evaluate the adsorption data.

$$\% R = \frac{c_0 - c_e}{c_0} \times 100\% \tag{1}$$

where  $C_0$  and  $C_c$  (mg L<sup>-1</sup>) are the initial and final concentrations of the Rhod B dye ve Ni (II) ions.

An equilibrium isotherm was used to demonstrate the removal efficiency of GO and GO-NH<sub>2</sub> and evaluated from its expression (qe vs. Ce). The adsorption behavior of adsorbents to RhodB dye Ni(II) metal ions was studied in depth based on the theory of adsorption isotherm (Langmuir, Freundlich, Dubinin–Radushkevich) and kinetic models (pseudo-first-order, pseudo-second-order, intraparticle diffusion, Boyd plot) using Originlab 9.0 software. The results were evaluated, the applicability of the model and the correlation coefficient ( $R^2$ ) of their linear fit were compared. The linear equations of the three models are presented below [19].

$$\frac{1}{q_e} = \frac{1}{K_L Q_M} \cdot \frac{1}{C_e} + \frac{1}{Q_M} \quad Langmuir \tag{2}$$

$$\log q_e = \log K_F + \frac{1}{n} \log C_e \text{ Freundlich}$$
(3)

$$\ln q_e = \ln q_s - k_{DR} \cdot \varepsilon^2 \text{ Dubinin-Radushkevich}$$
(4)  
where C<sub>e</sub> represents the equilibrium dye concentration (mg L<sup>-1</sup>); qe represents equilibrium and Q<sub>M</sub> represents the maximum

adsorption capacity (mg g<sup>-1</sup>);  $K_L$ ,  $K_E$  and  $k_{DR}$  represent the constants Langmuir, Freundlich and DR, respectively.  $\varepsilon$  and n indicate Polanyi potential and adsorption density, respectively [20,21]. The equilibrium parameter (also known as the separation factor;  $R_L$ ) was used to examine whether the adsorption process was positive or negative for the Langmuir adsorption model and was derived using Equation 5.

$$R_L = \frac{1}{1 + K_L C_0} \tag{5}$$

where the adsorption isotherm is considered positive ( $0 < R_L < 1$ ), negative ( $R_L > 1$ ), linear ( $R_L = 1$ ) and irreversible ( $R_L = 0$ ), respectively, depending on the R value.

$$E = (2k)^{-\frac{1}{2}}$$
(6)

The value of the average adsorption energy (E) gives information about whether the adsorption process is physical or chemical. If the E value is below 8 kJ mol<sup>-1</sup>, the adsorption process is called physical adsorption; when the E value is between 8 and 16 kJ mol<sup>-1</sup>, the adsorption process is called ion exchange or chemical adsorption [22].

Kinetic studies were carried out to determine the adsorption rate of Rhod B dye and Ni(II) ion from an aqueous solution; pseudo-first-order and pseudo-second-order. In addition, the intraparticle diffusion model and Boyd model were used to evaluate the transport mechanism. Equations representing the mentioned models are presented below [23].

$$\log(q_e - q_t) = \log q_e - \frac{k_1}{2.303} \cdot t \quad Pseudo-first \ order \tag{7}$$

$$\frac{t}{q} = \frac{1}{k_2 \cdot q_e^2} + \frac{1}{q_e} \cdot t \quad Pseudo-second \ order \tag{8}$$

$$q_{\rm c} = k_{\rm c} t^{1/2} + C$$
 Intraparticle diffusion (9)

$$Bt = -0.4977 - \ln(1 - F) Boyd model$$
(10)

 $F = \frac{q_t}{q_e}$ 

(11)

where  $k_1$ ,  $k_2$  and  $k_1$  represent pseudo-first-order, pseudo-second-order and intraparticle diffusion rate constant.  $q_e$  and  $q_t$  represent the amount of adsorption (mg g<sup>-1</sup>) at equilibrium and at any time t [24]. F represents the fraction of the adsorbate adsorbed at any time t, and B<sub>1</sub> is a mathematical function of F [25].

### 2.5. Desorption experiments

It was performed using distilled water and HCl as the desorption agent. Desorption was investigated by contacting 10 mg of dye/metal-loaded adsorbent with 50 mL of 0.1 M HCl. The dye/metal loaded samples were desorbed using 0.1 M HCl, washed with distilled water, dried and used for the next adsorption cycle.

### 3. Results and discussion

### 3.1. Characterization of GO and GO-NH<sub>2</sub>

In Figure 2, the DR-UV/vis and Raman spectrum of GO is given. For GO, the  $\pi \rightarrow \pi^*$  transition of the aromatic C-C ring and the  $n \rightarrow \pi^*$  transition of the C=O bond is seen at 232 and 306 nm, respectively [26]. In the Raman spectrum of GO in the range of 2500–500 cm<sup>-1</sup>, characteristic D and G bands were observed at 1330 and 1580 cm<sup>-1</sup>, respectively [27].

The broadening of the XRD spectra is due to the amorphous GO structure (Figure 3). In the obtained XRD spectra, characteristic peaks of the graphene oxide structure were observed at 23.8° and 43.1° as expected. In the XRD spectra of GO/Ni(II) and GO-NH<sub>2</sub>/Ni(II) structures, a prominent peak at (111) 44.9° assigned to the nickel ion was observed, but the characteristic peaks of nickel at 52° and 76° were not fully observed [28]. Since no significant change was observed in XRD intensities after dye adsorption, it was not evaluated.

As a result of the SEM images of the structures shown in Figure 4, the GO and  $\text{GO-NH}_2$  structures were found to be planar, and aggregation was observed upon adsorption of Ni(II) ions. Since no change was observed in the morphological structure after Rhod B dye adsorption, it was not evaluated.



Figure 2. DR-Uv/Vis and Raman spectra of GO.



**Figure 3.** XRD patterns of Ni (II) ions before-after adsorption onto GO and GO-NH,



**Figure 4.** SEM images of Ni (II) ions before-after adsorption onto GO (a-b) and GO-NH $_2$  (c-d).

In the FT-IR spectra given in Figure 5, the -OH vibrational band at  $3451-3342 \text{ cm}^{-1}$  in probable GO, C=O strong vibration band ( $1729-1707 \text{ cm}^{-1}$ ), C=C vibration band ( $1617-1579 \text{ cm}^{-1}$ ), CO (epoxy) vibration bands ( $1052-972 \text{ cm}^{-1}$ ) were observed. The vibration band of -OH/-NH in GO-NH<sub>2</sub> was observed at  $3393-3219 \text{ cm}^{-1}$ , C-H vibration band ( $3051-2921 \text{ cm}^{-1}$ ), weaker C=O vibration band ( $1696 \text{ cm}^{-1}$ ) were observed. C=C vibration band ( $1586 \text{ cm}^{-1}$ ), =C-H vibration band ( $1467-1389 \text{ cm}^{-1}$ ), Si-O-Si strong vibration band ( $1112 \text{ cm}^{-1}$ ) and Si-O-C vibration band ( $1046 \text{ cm}^{-1}$ ) were seen as expected. The strong C=O vibration band in the spectrum of GO is weakly seen in GO-NH<sub>2</sub>; the presence of strong Si-O-Si and Si-O-C vibration bands instead of C-O (epoxy) groups in the GO structure supports that the surface of the GO structure is functionalized with 3-aminopropyltriethoxysilane. It is known that graphene sheets contain functional hydroxyl groups in their basal planes and edges. These groups react with 3-aminopropyltriethoxysilane (APTES) to obtain a GO-NH<sub>2</sub> sample [29,30]. The functional -OH, -NH, -CO (epoxy), -C=O groups in the structure of GO-NH<sub>2</sub> predicted that can make a hydrogen bond or electrostatic interaction with metal ions (Ni <sup>2+</sup>) or rhodamine B dye (-COOH/-N(CH<sub>3</sub>) groups).

# 3.2. Adsorption results

# 3.2.1 Effect of contact time on the removal efficiency

Observation of the adsorption time is an essential step in elucidating the adsorption process and obtaining information about the nature of the adsorbent. In Figure 6, it is observed that the Rhod B and Ni (II) ion adsorption on GO did not change much over time, while the adsorption on  $\text{GO-NH}_2$  first reached equilibrium after a rapid increase. The adsorption of Rhod B dye was observed that stabilized after 30 min. It demonstrates that the Rhod B dye adsorption rate on  $\text{GO-NH}_2$  is relatively high, and there are many easily accessible sites. However, the adsorption of Ni(II) ions, equilibrium was observed at 200 min. As a result, the adsorption equilibrium time had been determined at 200 min as the optimum condition.

### 3.2.2 Effect of pH

The adsorption capacity of materials can be affected by the concentration of proton ions in an aqueous solution. Therefore, pH control is essential to capture the dye and metal ions in the adsorbate effectively. The optimum pH value also depends on the nature of the adsorbent used. For example, graphene oxide consists of various functional groups such as epoxy, hydroxyl, ketone, and carboxyl groups. When graphene oxide is dispersed in water, a negative charge is formed on its surface due to the ionization of its surface functional groups. While showing that the graphene oxide surface remains negatively charged in almost the entire pH range (pH<sub>pzc</sub> value above 2) [31], GO-NH<sub>2</sub> has a pH<sub>pzc</sub> of 3.8 [32]. The GO-NH<sub>2</sub> surface becomes negatively charged when the pH is higher than 3.8. In addition, the hydroxyl and carboxylic functional groups at the GO-NH<sub>2</sub> edges develop negative charges due to deprotonation [32,33]. The interaction between GO and GO-NH<sub>2</sub> adsorbents is a result of functional groups on the adsorbent surface and charges on dye molecules/heavy metal ions. Dyes are complex aromatic organic compounds with unsaturated bonds and various functional groups. Consequently, they have different ionization potentials at different pHs and cause a net charge change on the dye molecules [20].

In Figures 7a–7b, the effect of pH (pH = 2–9) on the adsorption of Rhod B dye and Ni (II) ions on GO and GO-NH<sub>2</sub> is presented. The pH of the solution affects the uptake of dye and heavy metal ions, as the surface charge of the adsorbent, the degree of ionization, and the type of adsorbate are affected. It is shown that solution pH significantly influences Ni (II) ions adsorption while it has little effect on rhodamine B adsorption. It was observed that the Rhod B dye removal, presented in Figure 7a, was largely unaffected by the increasing pH as pH increased from 2 to 9. Rhod B dye is a basic dye it contains a carboxyl group and the overall charge is positive. The reduction in Rhod B dye adsorption at pH 2 can be attributed to the electrostatic repulsion between the negatively charged surface and the Rhod B dye [34]. In addition, since the dye solution is not buffered, a change in the pH of the dye solution is expected during the sorption process. Further, while both the initial and equilibrium pH were initial pH = 4.83, the final pH was higher than the initial pH (6.58), indicating the possibility of either releasing OH<sup>-</sup> ions into the solution or removing H<sup>+</sup> ions from the solution [35].

The maximum adsorption removal of Ni(II) ions from GO and GO-NH<sub>2</sub> aqueous solution occurred at a pH between 4.5–7 (in Figure 7). Therefore, pH 6 was accepted as the optimum pH for further studies. The effect of pH can be explained by considering the surface charge on the adsorption material. At low pH, due to the high positive charge density due to protons in the surface regions, electrostatic repulsion will be increased during the uptake of metal ions, resulting in lower removal efficiency. With increasing pH, electrostatic repulsion decreases due to a decrease in positive charge density. Adsorption sites thus result in increased metal adsorption. The above fact about the effect of pH on adsorption has been supported by several previous researchers [36–38]. At higher pH values, OH<sup>-</sup> ions compete with active sites on the surface of adsorbents for Ni(II) [36]. Additionally, in the range above pH 8, nickel is present in the form of Ni(OH)<sup>+</sup> [39].

### 3.2.3 Effect of various ions

It contains various suspended and dissolved compounds that can be considered impurities in wastewater from the textile manufacturing or dyestuffs manufacturing industries. These impurities can be acids, alkalis, salts or metal ions. Cations such as Na<sup>+</sup>, K<sup>+</sup>, Cu<sup>2+</sup>, Ca<sup>2+</sup>, and Cr<sup>3+</sup> are the most common ions found in dye-containing wastewater [40].



Figure 5. FTIR spectra of GO and GO-NH<sub>2</sub>.



**Figure 6**. Effect of contact time (pH: 7;  $C_i = 30 \text{ mg } L^{-1}$ ; T = 298 K) on the adsorption of Rhod B dye (a) and Ni (II) ions (b) onto GO and GO-NH<sub>2</sub>.



**Figure 7.** Effect of pH ( $C_i$  = 30 mg L<sup>-1</sup>; t: 200 min; T = 298 K) on the adsorption of Rhod B dye and Ni (II) ions onto GO and GO-NH<sub>2</sub>.

In Figure 8, the effect of different ions  $(KNO_3, CaCO_3, Ca(NO_3)_2.4H_2O, NaCl and MnCl_2.H_2O)$  on the adsorption ability was observed. While the adsorption percentage does not decrease in Rhod B dye removal, a decrease is observed in Ni(II) ion removal. This decrease may be due to competition from other positively charged ions for the same binding sites on the adsorbent. Thus, the suitability of GO and GO-NH<sub>2</sub> for the ion exchange mechanism is supported in working environments with different ions [41].

#### 3.3. Adsorption isotherms

The equilibrium isotherm is of fundamental importance for the design and optimization of the adsorption system and it is necessary to establish the optimum correlation for the equilibrium curves. Because of comparing the linear fit and correlation coefficients (R<sup>2</sup>) of the three models presented in Table 1 and Figure 9, it can be said that the Langmuir isotherm model fits better than the Freundlich and D-R isotherm models.

The comparison of the  $Q_M$  maximum adsorption capacity (mg g<sup>-1</sup>) followed in the following order; for Rhod B; GO-NH<sub>2</sub> (3333 mg g<sup>-1</sup>) > GO (2500 mg g<sup>-1</sup>) > for Ni (II) ion; GO-NH<sub>2</sub> (714.28 mg g<sup>-1</sup>)> GO (312.5 mg g<sup>-1</sup>). In the Freundlich isotherm model, the 1/n value obtained for all adsorbents is below 1, which indicates the appropriate adsorption condition. The adsorption energy (E) represents the energy required for moving one mole of solute from infinity to the surface of the adsorbent. The adsorption energies (E) obtained from the DR isotherm model range between 0.707–1.0018 kJ mol<sup>-1</sup> at 298 K. Since E values are less than 8 kJ mol<sup>-1</sup>, the adsorption process of Rhod B and Ni (II) ions onto GO and GO-NH<sub>2</sub> is physical.

#### 3.4. Adsorption kinetics

According to the correlation coefficients ( $R^2$ ) presented in Table 2 and Figure 10, the pseudo-second-order (PSO) kinetic model fits better. It was also found that the  $q_{e(cal)}$  values obtained from the pseudo-second-order (PSO) kinetic model were comparable to  $q_{e(exp)}$  compared to the pseudo-first-order (PFO) kinetic model. Since it could not be determined that the step controlling the adsorption rate from the PFO and PSO kinetic models was film or pore diffusion, the kinetic data were also analyzed and interpreted with the intraparticle diffusion model and the Boyd model [21].



**Figure 8.** Effect of various ions for Rhod B dye (a) and Ni (II) ions adsorption ( $C_i = 0.3 \text{ M}$  (strange ions);  $C_i = 30 \text{ mg L}^{-1}$  (dye/metal ions); T = 298 K; pH = 6.5).

 Table 1. Adsorption isotherm parameters.

Isotherm models		Rhod B		Ni(II)	
		GO	GO-NH <sub>2</sub>	GO	GO-NH <sub>2</sub>
Langmuir	$Q_{M}(mg g^{-1})$	2500	3333	312.5	714.28
	K	0.0013	0.0003	0.0012	0.0007
	R <sub>L</sub>	0.9447	0.9867	0.9488	0.9694
	R <sup>2</sup>	0.9999	0.9899	0.9101	0.9895
Freundlich	K <sub>F</sub>	1.8958	1.0018	3.1318	2.1967
	1/n	0.9969	0.9803	0.9730	0.9569
	R <sup>2</sup>	0.9999	0.9844	0.9214	0.9855
Dubinin-	$q_{M} (mg g^{-1})$	2189	2464	178.3	393.03
Radushkevich	K <sub>D-R</sub>	1.E-6	5.E-7	1.E-6	1.E-6
	E <sub>D-R</sub>	0.707	1.001	0.756	0.707
	R <sup>2</sup>	0.9374	0.8551	0.7495	0.8903

 Table 2. Value of constants of various kinetic models.

Kinetic		Rhodamine B		Ni (II) ions	
Models		GO	GO-NH <sub>2</sub>	GO	GO-NH <sub>2</sub>
	$q_{e(exp)}(mgg^{-1})$	67.6269	74.7501	68.4926	7.4903
Pseudo-first order	q <sub>e. (cal)</sub> (mg g-1)	2.4216	2.8511	6.3489	4.9843
	k <sub>1</sub> (min-1)	0.0145	0.0070	0.7121	0.0689
	R <sup>2</sup>	0.9794	0.3426	0.5285	0.8743
Pseudo-second order	q <sub>e. (cal)</sub> (mg g-1)	66.6660	75.1880	73.5294	75.7576
	$k_2(g mg^{-1} min-1)$	0.0122	0.2211	0.0022	0.0020
	R <sup>2</sup>	1.0000	1.0000	0.9947	0.9957





Figure 9. Adsorption isotherm models for Rhod B; GO (a-d):GO-NH<sub>2</sub>(e-h) and Ni(II) ions; GO (1-l):GO-NH<sub>2</sub>(m-p).



**Figure 10.** Adsorption kinetic models for Rhod B; GO and Go- $NH_2$  (a) and Ni(II) ions; GO and Go- $NH_2$  (b).

An adsorption process can be completed by either transduction, film or intraparticle diffusion (diffusion of the adsorbent within the pores) or film diffusion and intraparticle diffusion. The kinetic data were fitted to the intraparticle diffusion model and it was observed that the graph did not pass through the origin. It indicates that intraparticle diffusion was not the only rate-limiting step. According to the lines set in Figure 11, the first stage is the transport of adsorbate molecules to the outer surface of the adsorbent (film diffusion) and the second stage; represents the intraparticle diffusion of the adsorbent into its pores. In the third stage, the adsorbate was adsorbed to the inner region of the adsorbent [42]. The third stage was not considered a rate-limiting step as it is comparatively faster than the other two stages. It explains that this adsorption process fits this model well since most correlation coefficients ( $R^2$ ) were higher than 0.90. In Figure 9, Rhod B dye adsorption on GO-NH<sub>2</sub> occurred in two steps; other adsorption processes occurred in three stages. A lower slope corresponds to a slower adsorption process. For this reason, it is concluded that the film diffusion steps were the rate-limiting step in the adsorption process [43].

Boyd plots with Bt versus t plot were obtained using Equations 9 and 10. A straight plot through the origin means that the adsorption process is controlled by intraparticle diffusion. Otherwise, the adsorption process is controlled by film diffusion or both film and intraparticle diffusion. From the experimental results, the plots of Boyd's equation were nonlinear and did not pass through the origin (Figure 12). As a result, both models support that the rate-limiting step of the adsorption process is film diffusion [23,44].

### 3.6. Desorption

Desorption studies are essential to elucidate the nature of the adsorption process and to recover the adsorbent. Since the adsorption process's economics depends on the adsorbents' regeneration, its practical application is indispensable for industries [41]. As shown in Figure 13, the adsorption/desorption cycles were repeated three times. The results can conclude that although the adsorption capacity decreases slightly after each cycle, the synthesized GO and GO-NH<sub>2</sub> can be used repeatedly with negligible loss of adsorption capacity for dye and metal ions.

### 3.7. Adsorption mechanism

Adsorption is a surface phenomenon in which adsorbates (ions or molecules) are held together by van der Waals forces (physisorption) or by forming chemical bonds (chemical adsorption) [45]. Also, adsorption mechanisms resulting from the electrostatic interaction, hydrogen bonding and  $\pi$ - $\pi$  interaction have been reported as the primary mechanisms for graphene-based adsorbents to remove organic dyes [46]. Interestingly, various types of forces such as H-bonds, electrostatic interactions, ion exchange and  $\pi$ - $\pi$  interactions are responsible for physical adsorption [47]. For example, GO carries many functional groups, such as carboxylic acids, that can readily release protons in water and cause an adsorbent surface to charge. In this case, the adsorption is probably governed by electrostatic interactions. Since GO-NH<sub>2</sub> has various oxygencontaining active functional groups such as hydroxyl, carbonyl and epoxy groups, it can be adsorbed via (a) ion exchange, (b) surface complexation, and (c) electrostatic attraction [32]. The decrease in the intensity of the v(C=O) peak and the broadening of the v(OH) peak in the FTIR spectrum (Figure 14) also confirm the binding of these functional groups via electrostatic attraction process might occur due to the  $\pi$ - $\pi$  stacking interaction of the aromatic ring of the rhodamine B dye with the nanolayers of GO samples. In this study, physisorption can be attributed to the adsorption of dye (Rhod B) and heavy metal (Ni (II) ions) ions on GO and GO-NH<sub>2</sub> (Figure 15).

### 3.8. Comparison with other adsorbents

In Table 3, the adsorption capacities of other adsorbents used to remove Rhod B dye and Ni (II) ions from an aqueous solution were compared. After functionalizing both adsorbents with high efficiency, especially with the  $-NH_2$  group, their active areas increased and their performance improved.



Figure 11. Intraparticle diffusion models for Rhod B; GO (a), Go-NH $_2$  (b), and Ni(II) ions; GO (c) and Go-NH $_2$  (d).

Table 3. Comparison of different adsorbents for removal of Rhod B. dye and Ni (II) ions.	

Adsorbent	Adsorbate	Adsorption capacity $(q_M)$	Isotherms	Ref.
Waste seeds Aleurites moluccana (WAM)	Rhod. B	117 (mg g-1)	Sip	[2]thermogravimetric analysis (TGA
ZSM-5 Synthesized from Bangka kaolin	Rhod. B	128.21 (mg g-1)	Langmuir	[48]
Activated carbon	Rhod. B	255.39 (mg g-1)	Langmuir	[49]
UiO-66-(COOH)2	Rhod. B	2200 (mg g-1)	Langmuir	[50]
GO-NH <sub>2</sub>	Rhod. B	3333 (mg g-1)	Langmuir and Freundlich	This study
Nano kaolinite	Ni(II) ions	111 (mg g-1)	Langmuir	[51]
Rice husk (microwave-functionalized cellulose)	Ni(II) ions	80.38 (mg g-1)	Langmuir	[52]microwave- functionalized cellulose derived from rice husk was cost-effectively prepared and employed for Pb(II
Hydrogel	Ni(II) ions	286.7 (mg g-1)	Langmuir	[53]
Chitosan (CS) (CS-g-AOPAM)	Ni(II) ions	213.4 (mg g-1)	Langmuir	[54]
GO-NH <sub>2</sub>	Ni(II) ions	714.28 (mg g-1)	Langmuir and Freundlich	This study



Figure 12. Boyd models for Rhod B; GO, GO-NH, (a) and Ni(II) ions; GO, Go-NH, (b).



**Figure 13**. The performance of GO and  $\text{GO-NH}_2$  for three cycles of adsorption-regeneration for Rhod B dye and Ni (II) ions (pH = 7).



**Figure 14.** FTIR spectrum of GO-NH<sub>2</sub>, GO-NH<sub>2</sub>-NiCl<sub>2</sub> and GO-NH<sub>2</sub>-Rhod B structures.



Figure 15. Schematic representation of Rhod B and Ni (II) ions on the GO, GO-NH, surface.

# 4. Conclusions

In this study, GO and amino-functionalized GO (GO-NH<sub>2</sub>) were synthesized by the Hummers method to investigate the adsorption properties of Rhod B dye and Ni (II) ions. Maximum adsorption capacities of Rhod B dye and Ni (II) ion on GO and GO-NH<sub>2</sub> are 2500, 3333, 312.5, and 714.28 mg g<sup>-1</sup> at optimal pH = 6 values, respectively, the adsorption kinetics agreed well with the pseudo-second-order kinetic model. The sorption isotherms are compatible with the Langmuir model. The maximum removal efficiency (99.9%) was obtained for Rhod B dye in industrial wastewater with GO-NH<sub>2</sub>. The adsorption-desorption results showed that the reusability of GO and GO-NH<sub>2</sub> is encouraging and effective in dye and metal removal. The easy separation of Rhod B dye and Ni (II) ions from charged GO and GO-NH<sub>2</sub> samples using HCl acid solution shows that the adsorption mechanism could be explained by physisorption.

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# Credit authorship contribution statement

Eda Gökırmak Söğüt: Funding acquisition, formal analysis, writing-original draft, writing-review & editing. Metin Çelebi: Conceptualization, formal analysis, writing- original draft, writing-review & editing

### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

### References

- 1. Velusamy S, Roy A, Sundaram S, Mallick TK. A Review on Heavy Metal Ions and Containing Dyes Removal Through Graphene Oxide-Based Adsorption Strategies for Textile Wastewater Treatment. The Chemical Record 2021; 21 (7): 1570-1610. doi: 10.1002/tcr.202000153
- 2. Postai DL, Demarchi CA, Zanatta F, Melo DCC, Rodrigues CA. Adsorption of rhodamine B and methylene blue dyes using waste of seeds of Aleurites Moluccana, a low cost adsorbent. Alexandria Engineering Journal 2016; 55 (2): 1713-1723. doi: 10.1016/j.aej.2016.03.017
- 3. Rani P, Johar R, Jassal PS. Adsorption of nickel (II) ions from wastewater using glutaraldehyde cross-linked magnetic chitosan beads: isotherm, kinetics and thermodynamics. Water Science and Technology 2020; 82 (10): 2193-2202. doi: 10.2166/wst.2020.459
- 4. Lellis B, Fávaro-Polonio CZ, Pamphile JA, Polonio JC. Effects of textile dyes on health and the environment and bioremediation potential of living organisms. Biotechnology Research and Innovation 2019; 3 (2): 275-290. doi: 10.1016/j.biori.2019.09.001
- Zhang X, Wang X. Adsorption and Desorption of Nickel(II) Ions from Aqueous Solution by a Lignocellulose/Montmorillonite Nanocomposite. PLOS ONE 2015; 10 (2): e0117077. doi: 10.1371/journal.pone.0117077
- 6. Oyekanmi AA, Ahmad A, Hossain K, Rafatullah M. Adsorption of Rhodamine B dye from aqueous solution onto acid treated banana peel: Response surface methodology, kinetics and isotherm studies. PLOS ONE 2019; 14 (5): e0216878. doi: 10.1371/journal.pone.0216878
- 7. De Gisi S, Lofrano G, Grassi M, Notarnicola M. Characteristics and adsorption capacities of low-cost sorbents for wastewater treatment: A review. Sustainable Materials and Technologies 2016; 9 : 10-40. doi: 10.1016/j.susmat.2016.06.002
- Theron J, Walker JA, Cloete TE. Nanotechnology and water treatment: Applications and emerging opportunities. Critical Reviews in Microbiology 2008; 34 (1): 43-69. doi: 10.1080/10408410701710442
- 9. Gehrke I, Geiser A, Somborn-Schulz A. Innovations in nanotechnology for water treatment. Nanotechnology, Science and Applications 2015; 8: 1. doi: 10.2147/nsa.s43773
- 10. Madadrang CJ, Kim HY, Gao G, Wang N, Zhu J, et al. Adsorption behavior of EDTA-graphene oxide for Pb (II) removal. ACS Applied Materials and Interfaces 2012; 4 (3): 1186-1193. doi: 10.1021/am201645g
- 11. Zhang X, Qin C, Gong Y, Song Y, Zhang G, et al. Co-adsorption of an anionic dye in the presence of a cationic dye and a heavy metal ion by graphene oxide and photoreduced graphene oxide. RSC Advances 2019; 9 (10): 5313-5324. Accessed June 22, 2021. https://pubs.rsc. org/en/content/articlehtml/2019/ra/c8ra09438a
- 12. Soğukömeroğulları HG, Karataş Y, Celebi M, Gülcan M, Sönmez M, et al. Palladium nanoparticles decorated on amine functionalized graphene nanosheets as excellent nanocatalyst for the hydrogenation of nitrophenols to aminophenol counterparts. Journal of Hazardous Materials 2019; 369: 96-107. doi: 10.1016/j.jhazmat.2019.02.027
- 13. Xing HT, Chen JH, Sun X, Huang YH, Su ZB, et al. NH2-rich polymer/graphene oxide use as a novel adsorbent for removal of Cu(II) from aqueous solution. Chemical Engineering Journal 2015; 263: 280-289. doi: 10.1016/j.cej.2014.10.111
- 14. Wang S, Li X, Liu Y, Zhang C, Tan X, et al. Nitrogen-Containing Amino Compounds Functionalized Graphene Oxide: Synthesis, Characterization and Application for the Removal of Pollutants from Wastewater: A Review. Vol 342.; 2018:177-191.
- 15. Luo S, Xu X, Zhou G, Liu C, Tang Y, et al. Amino siloxane oligomer-linked graphene oxide as an efficient adsorbent for removal of Pb(II) from wastewater. Journal of Hazardous Materials 2014; 274: 145-155. doi: 10.1016/j.jhazmat.2014.03.062
- Olanipekun O, Oyefusi A, Neelgund GM, Oki A. Synthesis and characterization of reduced graphite oxide-polymer composites and their application in adsorption of lead. Spectrochimica Acta - Part A: Molecular and Biomolecular Spectroscopy 2015; 149: 991-996. doi: 10.1016/j.saa.2015.04.071
- 17. Firdaus RM, Rosli NIM, Ghanbaja J, Vigolo B, Mohamed AR. Enhanced adsorption of methylene blue on chemically modified graphene nanoplatelets thanks to favorable interactions. Journal of Nanoparticle Research 2019 21:12 2019; 21 (12): 1-18. doi: 10.1007/s11051-019-4701-4
- Bulut A, Yurderi M, Ertas IE, Celebi M, Kaya M, et al. Carbon dispersed copper-cobalt alloy nanoparticles: A cost-effective heterogeneous catalyst with exceptional performance in the hydrolytic dehydrogenation of ammonia-borane. Applied Catalysis B: Environmental 2016; 180: 121-129. doi: 10.1016/j.apcatb.2015.06.021
- Kul AR, Söğüt EG, Kılıç NÇ. Adsorption of Neutral Red Dye from Aqueous Solutions by Natural Adsorbent: An Equilibrium, Kinetic And Thermodynamic Study. Commun Fac Sci Univ Ank Ser B Chemistry and Chemical Engineering 2021; 63 (1): 27-60. Accessed October 29, 2021. https://dergipark.org.tr/en/pub/communb/issue/64811/948429
- 20. Sharma G, Kumar A, AlGarni TS, Naushad M, et al. Adsorption of cationic dyes onto carrageenan and itaconic acid-based superabsorbent hydrogel: Synthesis, characterization and isotherm analysis. Journal of Hazardous Materials 2022; 421: 126729. doi: 10.1016/j.jhazmat.2021.126729
- 21. Gökırmak E, Çalışkan N. The effect of mercapto-functionalization of thermo-acid activated diatomite for dye removal from aqueous solutions. International Journal of Environmental Analytical Chemistry 2020; 00: 1-27. doi: 10.1080/03067319.2020.1849645

- 22. Gökırmak E, Çalışkan N. Isotherm and Kinetic Studies of Pb(II) Adsorption on Raw And Modified Diatomite By Using Non-Linear Regression Method. Fresenius Environmental Bulletin 2017; 26 (4): 2720-2728.
- Gökırmak E, Karataş Y, Gülcan M, Kılıç NÇ. Enhancement of adsorption capacity of reduced graphene oxide by sulfonic acid functionalization: Malachite green and Zn (II) uptake. Materials Chemistry and Physics 2020; 256: 123662. doi: 10.1016/j. matchemphys.2020.123662
- 24. Hossain MY, Zhu W, Pervez MN, Yang X, Sarker S, et al. Adsorption, kinetics, and thermodynamic studies of cacao husk extracts in waterless sustainable dyeing of cotton fabric. Cellulose 2021 28:4 2021; 28 (4): 2521-2536. doi: 10.1007/s10570-020-03662-0
- 25. Kumar PS, Senthamarai C, Durgadevi A. Adsorption kinetics, mechanism, isotherm, and thermodynamic analysis of copper ions onto the surface modified agricultural waste. Environmental Progress & Sustainable Energy 2014; 33 (1): 28-37. doi: 10.1002/ep.11741
- 26. Bhowmik K, Mukherjee A, Mishra MK, De G. Stable ni nanoparticle-reduced graphene oxide composites for the reduction of highly toxic aqueous Cr(VI) at room temperature. Langmuir 2014; 30 (11): 3209-3216. doi: 10.1021/la500156e/suppl\_file/la500156e\_si\_001.pdf
- 27. Liu X, Pan L, Zhao Q, Lv T, Zhu G, et al. UV-assisted photocatalytic synthesis of ZnO–reduced graphene oxide composites with enhanced photocatalytic activity in reduction of Cr(VI). Chemical Engineering Journal 2012; 183: 238-243. doi: 10.1016/j.cej.2011.12.068
- Li W, Ren J, Zhao XY, Takarada T. H2 and Syngas Production from Catalytic Cracking of Pig Manure and Compost Pyrolysis Vapor over Ni-Based Catalysts. Polish Journal of Chemical Technology 2018; 20 (3): 8-14. doi: 10.2478/pjct-2018-0032
- 29. Lin Y, Jin J, Song M. Preparation and characterisation of covalent polymer functionalized graphene oxide. Journal of Materials Chemistry 2011; 21 (10): 3455-3461. doi: 10.1039/c0jm01859g
- 30. Serodre T, Oliveira NAP, Miquita DR, Ferreira MP, Santos AP, et al. Surface Silanization of Graphene Oxide Under Mild Reaction Conditions. Journal of the Brazilian Chemical Society 2019; 30 (11): 2488-2499. doi: 10.21577/0103-5053.20190167
- Sahar J, Naeem A, Farooq M, Zareen S, Urrahman A. Thermodynamic studies of adsorption of rhodamine b and congo red on graphene oxide. Desalination and Water Treatment 2019; 164 : 228-239. doi: 10.5004/dwt.2019.24436
- 32. Huang H, Wang Y, Zhang Y, Niu Z, Li X. Amino-functionalized graphene oxide for Cr(VI), Cu(II), Pb(II) and Cd(II) removal from industrial wastewater. Open Chemistry 2020; 18 (1): 97-107. doi: 10.1515/chem-2020-0009
- 33. Kumar M, Chung JS, Hur SH. Graphene Composites for Lead Ions Removal from Aqueous Solutions. Applied Sciences 2019; 9 (14): 2925. doi: 10.3390/app9142925
- Mchedlov-Petrossyan NO, Vodolazkaya NA, Doroshenko AO. Ionic Equilibria of Fluorophores in Organized Solutions: The Influence of Micellar Microenvironment on Protolytic and Photophysical Properties of Rhodamine B. Journal of Fluorescence 2003; 13 (3): 235-248. doi: 10.1023/a:1025089916356
- Maurya NS, Mittal AK, Cornel P, Rother E. Biosorption of dyes using dead macro fungi: Effect of dye structure, ionic strength and pH. Bioresource Technology 2006; 97 (3): 512-521. doi: 10.1016/j.biortech.2005.02.045
- 36. Hannachi Y, Shapovalov NA, Hannachi A. Adsorption of Nickel from aqueous solution by the use of low-cost adsorbents. 2010; 27 (1): 152-158. Accessed December 13, 2021. https://link.springer.com/article/10.1007/s11814-009-0303-7
- 37. Cruz-Lopes LP, Macena M, Esteves B, Guiné RPF. Ideal pH for the adsorption of metal ions Cr6+, Ni2+, Pb2+ in aqueous solution with different adsorbent materials. Open Agriculture 2021; 6 (1): 115-123. doi: 10.1515/opag-2021-0225
- Ciesielczyk F, Bartczak P, Wieszczycka K, Siwińska-Stefańska K, Nowacka M, et al. Adsorption of Ni(II) from model solutions using coprecipitated inorganic oxides. Adsorption 2013 19:2 2013; 19 (2): 423-434. doi: 10.1007/s10450-012-9464-5
- Jhonatan R., Guarín-Romero Paola, Rodríguez-Estupiñán Liliana G, Moreno-Piraján JC. Simple and Competitive Adsorption Study of Nickel(II) and Chromium(III) on the Surface of the Brown Algae Durvillaea antarctica Biomass. ACS Omega 2019; 4 (19): 18147-18158. doi: 10.1021/acsomega.9b02061
- 40. Correia VM, Stephenson T, Judd SJ. Characterisation of textile wastewaters a review. Http://dx.doi.org/101080/09593339409385500 2008; 15 (10): 917-929. doi: 10.1080/09593339409385500
- 41. Qasem NAA, Mohammed RH, Lawal DU. Removal of heavy metal ions from wastewater: a comprehensive and critical review. Npj Clean Water 2021 4:1 2021; 4 (1): 1-15. doi: 10.1038/s41545-021-00127-0
- 42. Huang Y, Lee X, Grattieri M, Macazo FC, Cai R, et al. A sustainable adsorbent for phosphate removal: modifying multi-walled carbon nanotubes with chitosan. Journal of Materials Science 2018 53:17 2018; 53 (17): 12641-12649. doi: 10.1007/s10853-018-2494-y
- Cheung WH, Szeto YS, McKay G. Intraparticle diffusion processes during acid dye adsorption onto chitosan. Bioresource Technology 2007; 98 (15): 2897-2904. doi: 10.1016/j.biortech.2006.09.045
- 44. Yao C, Chen T. A film-diffusion-based adsorption kinetic equation and its application. Chemical Engineering Research and Design 2017; 119: 87-92. doi: 10.1016/j.cherd.2017.01.004

- 45. Ahmed A, Ali A, Ahmed M, Parida KN, Ahmad M, et al. Construction and topological studies of a three dimensional (3D) coordination polymer showing selective adsorption of aromatic hazardous dyes. Separation and Purification Technology 2021; 265: 118482. doi: 10.1016/j.seppur.2021.118482
- 46. Mutolib Bankole O, Oyeneyin OE, Olaseni E, Akeremale OK, Adanigbo P, et al. Kinetics and Thermodynamic Studies for Rhodamine B Dye Removal onto Graphene Oxide Nanosheets in Simulated Wastewater. Http://www.sciencepublishinggroup.com 2019; 7 (1): 10. doi: 10.11648/j.ajac.20190701.12
- Dhotel A, Chen Z, Delbreilh L, Youssef B, Saiter JM, et al. Molecular Motions in Functional Self-Assembled Nanostructures. International Journal of Molecular Sciences 2013; 14 (2): 2303. doi: 10.3390/ijms14022303
- 48. Iryani A, Nur H, Santoso M, Hartanto D. Adsorption study of rhodamine B and methylene blue dyes with ZSM-5 directly synthesized from Bangka Kaolin without organic template. Indonesian Journal of Chemistry 2020; 20 (1): 130-140. doi: 10.22146/ijc.41369
- 49. Abdolrahimi N, Tadjarodi A. Adsorption of Rhodamine-B from Aqueous Solution by Activated Carbon from Almond Shell. Proceedings 2019; 41: 51. doi: 10.3390/ecsoc-23-06619
- 50. Gao X, Zheng M, Zhao X, Song S, Gao Z. Ultra-High-Capacity Adsorption of Rhodamine B in a Carboxyl-Functionalized Metal–Organic Framework via Surface Adsorption. Journal of Chemical & Engineering Data 2020; 66 (1): 669-676. doi: 10.1021/acs.jced.0c00818
- 51. Alasadi AM, Khaili FI, Awwad AM. Adsorption of Cu(II), Ni(II) and Zn(II) ions by nano kaolinite: Thermodynamics and kinetics studies. Chemistry International 2019; 5 (4): 258-26. doi: 10.5281/zenodo.2644985
- Qu J, Tian X, Jiang Z, Cao B, Akindolie MS, et al. Multi-component adsorption of Pb(II), Cd(II) and Ni(II) onto microwave-functionalized cellulose: Kinetics, isotherms, thermodynamics, mechanisms and application for electroplating wastewater purification. Journal of Hazardous Materials 2020; 387: 121718. doi: 10.1016/j.jhazmat.2019.121718
- 53. Wang Z, Li TT, Peng HK, Ren HT, Lou CW, et al. Low-cost hydrogel adsorbent enhanced by trihydroxy melamine and β-cyclodextrin for the removal of Pb(II) and Ni(II) in water. Journal of Hazardous Materials 2021; 411: 125029. doi: 10.1016/j.jhazmat.2020.125029
- 54. Tang L, Gou S, He Y, Liu L, Fang S, et al. An efficient chitosan-based adsorption material containing phosphoric acid and amidoxime groups for the enrichment of Cu(II) and Ni(II) from water. Journal of Molecular Liquids 2021; 331: 115815. doi: 10.1016/j.molliq.2021.115815